

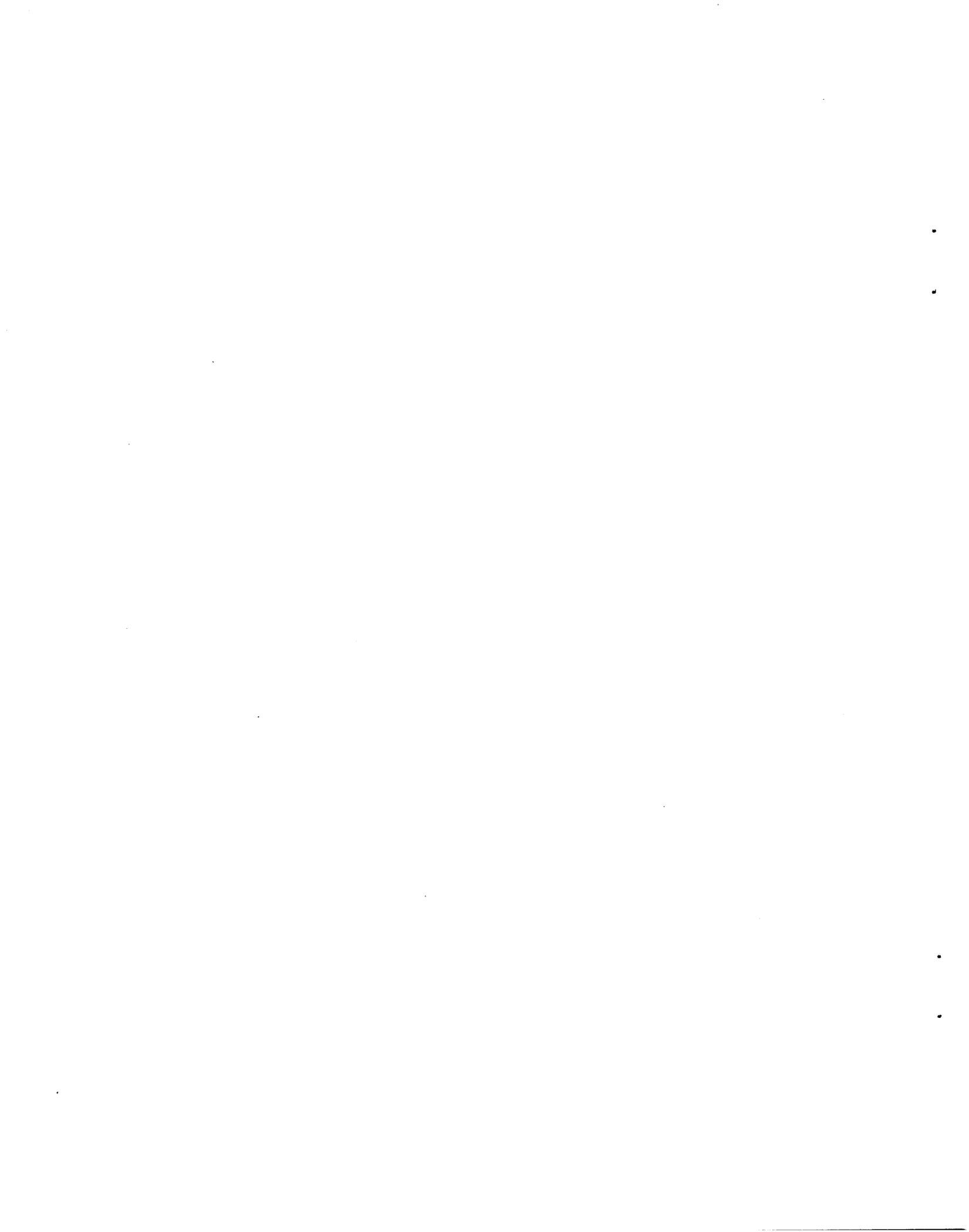
A Framework for Utilizing Fire Property Tests

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NIST



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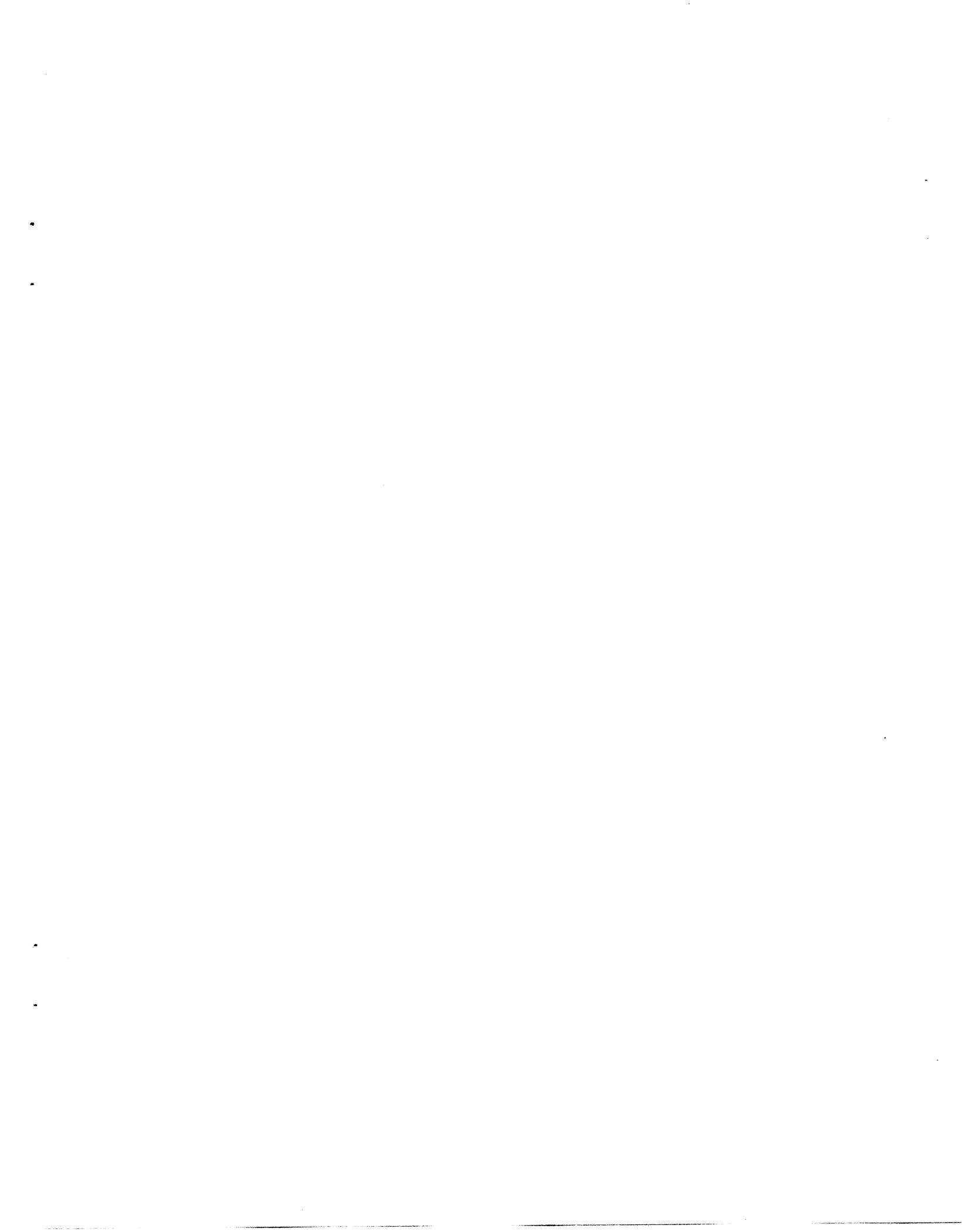


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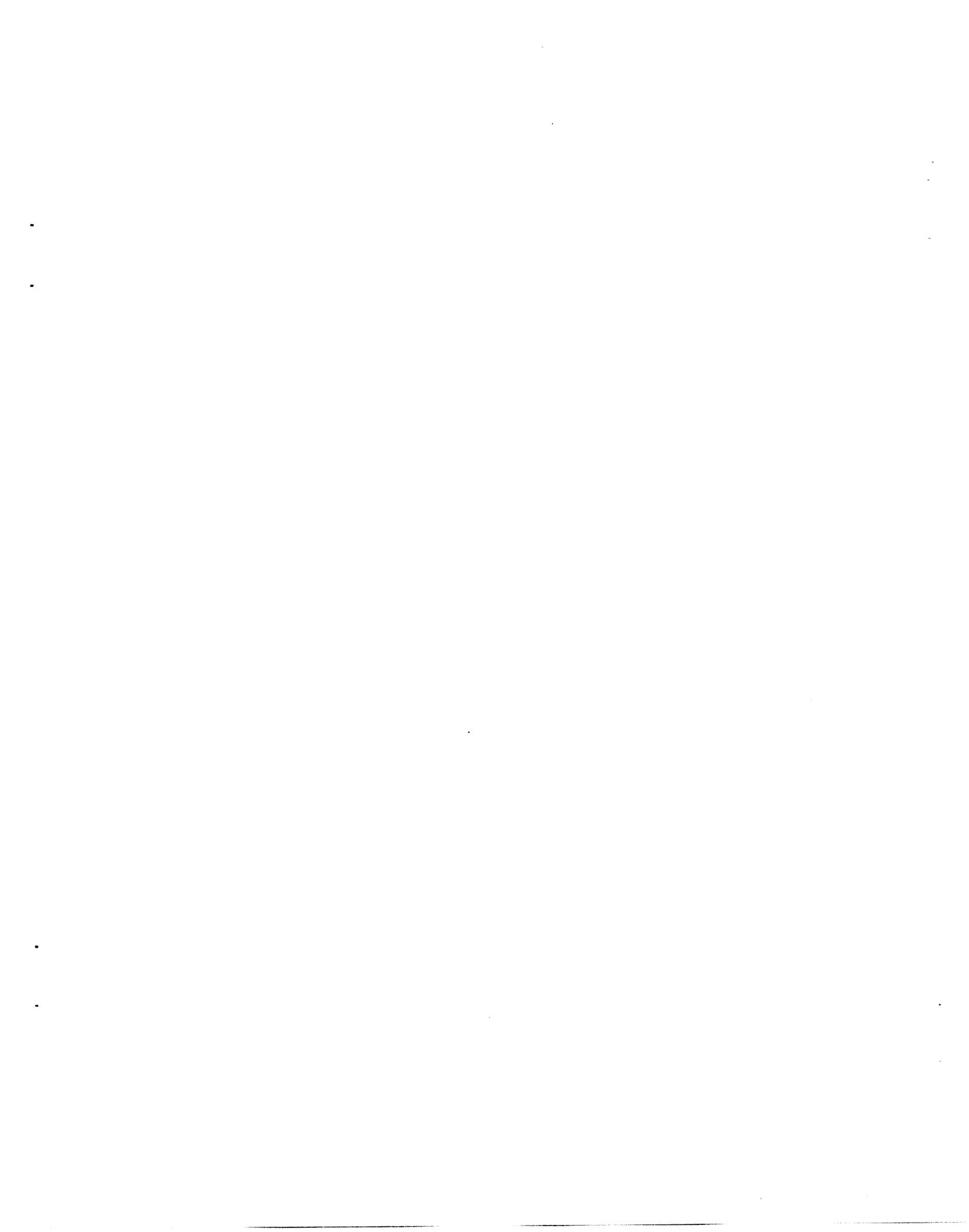
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ABSTRACT

A complete approximate set of equations is developed to describe fire spread over a surface and its resultant energy release. Wall, floor, and ceiling orientations are considered. The needed model data are couched in terms of available test method results, e.g., Cone Calorimeter and LIFT apparatuses. Several applications are presented to show how energy release rates can be predicted and how well they represent real data from full-scale and model room lining experiments.

Key Words: Heat release, flammability tests, fire prediction, linings, room fires.

1. INTRODUCTION

Traditionally, fire test methods have been used to provide relative rankings of material and product performance from which officials have defined safety requirements. This process has been empirical relying on judgement and fire experience. Although, one would expect fire safety to be consistent, each regulatory agency or government has laid out its own tests and procedures creating an array of different results. Test methods stand more on their longevity, than on their scientific merits. This is an unsound technical situation which can compromise safety. The solution to this state of affairs is, however, not readily accessible since a technical consensus has not yet been developed from the science of fire. Hence, a complete scientific alternative is not yet possible, but a framework for an alternative can be developed in terms of available scientific information and methods. We will present such a framework and demonstrate its utility and level of accuracy.

Theories of flame spread and new widely used test apparatuses capable of providing engineering fire property data make it feasible to construct a framework for fire hazard assessment. The test apparatuses include the Cone Calorimeter [1], and the Lateral Ignition and Flame Spread Test (LIFT) [2], both of which have been recently established as ASTM standard methods and are being considered in ISO. We shall not review the details of these apparatuses here, it only suffices that they can produce the needed data in the analysis to follow. That analysis will be confined to fire growth on flat materials in applications of floors, walls and ceilings. We shall formulate a model to compute the "output" of the fire growth as a function of time in terms of the material orientation and properties. The "output" can be defined as appropriate for the hazard. In the exercises to follow we shall address the output as energy release rate representative of the hazard of rapid fire growth or perhaps flashover.

The model to be presented, we emphasize, represents only a framework for a more complete and precise solution to the appropriate characterization of materials through fire test methods. But once formulated, we tested the model against various data sets for full scale behavior of fire growth on lining materials in rooms. Our results and our model should serve as support for other analyses which have used similar property data to predict the flashover times for some of these experiments [3-5]. However, we believe that our model is less empirical and more physically complete than these previous analyses [3-5], and the accuracy of the end results is comparable. Indeed, it suggests that we all have selected the key properties in our analyses which illustrates the value of the new fire property tests in supplying useful and versatile engineering data. Hence, future models should be able to build improvement on this base. Finally, our model will be capable of coping with changing environmental conditions, but we shall not implement this in any dynamic sense by coupling its fire growth to the changing conditions of a room involved in fire. However, we will examine some effects of pre-heating during flame spread that could come as a result of thermal feedback due to a confined fire.

2. THEORETICAL DEVELOPMENT

Initially the purpose of the analysis to follow was to illustrate how fire property test data could be used in modeling to yield meaningful quantitative results for assessing fire safety. As will be seen, the use of the analysis is capable of producing very accurate results. This probably resulted from our approach of keeping the model simple but complete. We have included the essential elements of fire growth; namely, ignition, energy release rate, burning time, and all relevant modes of flame spread for the surface orientation considered. Also, we have included effects of the ignition fire source, and have considered parametrically, the effects of thermal feedback. Detailed transient characteristics and room smoke layering have been ignored, but these effects could easily be included in a more refined analysis and their contributions assessed. However, it can be argued that their impact is likely to be secondary, but ultimately needs to be examined.

Fire Properties:

The term "fire properties" has been used, but we need to define it in context. Generally, engineering property data constitute physical and chemical parameters, usually arising from thermodynamic principles or rate process models. Although we could couch our analysis in terms of such true properties, we choose to use more directly measurable quantities since fire modeling is not yet complete enough to deal with complex materials. Hence, our "fire properties" will not necessarily be valid engineering properties and will depend on environmental conditions. We will identify these "fire properties" as we develop our theory. As an introduction, we list them now:

1. \bar{Q}'' , average peak heat release rate per unit area

This value is derived from a device like the Cone Calorimeter [1] for which the transient data have been averaged, and evaluated at a specified irradiance level. It is illustrated in Figure 1 in which the area under the actual curve is approximately equal to the area under the rectangle. We have not used a standardized prescription for determining the average energy release rate and burn time. This was done in a consistent manner by approximating the significant burning region of the curve by a square wave. We selected an average maximum for \bar{Q}'' and then estimated t_b to maintain the total energy.

2. t_b , burn time

This value is the width of the approximating rectangle in Figure 1. This also corresponds to a given heat flux, and is derivable from the Cone Calorimeter.

3. t_{ig} , ignition time

This value is the time for piloted ignition at a given heat flux, specifically radiative. The heat flux level should be selected to correspond to the flame heat flux level appropriate to wind-aided flame spread. This will be defined more specifically later. This "property" can be derived from a number of ignition apparatuses without any loss in uniqueness since it should not be very dependent on the apparatus (e.g., Cone Calorimeter [1], [2]) provided the radiant emission spectrum of the apparatus is similar.

4. Φ , flame heating parameter in opposed flow spread

This "property" is directly derivable from the LIFT [2,6] standard procedure. It represents the flame heat transfer and opposed flow velocity effects. In the LIFT mode, the flow velocity corresponds to a natural convection condition, and experience suggests that the Φ is not strongly sensitive to surface orientation.

5. $T_{s,min}$, minimum temperature for flame spread

In opposed flow flame spread it is found that, in general, materials require a minimum heating level to achieve a surface temperature required for spread. Below this temperature spread is not possible. Above this temperature and up to the ignition temperature (T_{ig}) of the material is the domain of surface

temperatures where surface flame spread theory applies. For external heating conditions that lead to the attainment of the ignition temperature, a gas-phase flammable mixture can result with flame propagation still possible as is a "gas-phase" phenomenon in contrast to surface spread that we are considering here. Although this property, $T_{s,min}$, can be derived from the LIFT for opposed flow spread, it is also required but not available for, wind-aided or upward flame spread. For example, it appears that a pre-heated surface temperature in excess of 80°C is necessary to cause sustained upward flame spread on wood particle board [7].

Equations:

In developing the governing equations we shall consider all materials to be thermally thick, i.e. no effect of thickness, and laminated materials and substrates are treated as homogeneous, reflective of their bulk properties. The same corresponding equations will apply, without distinction, to horizontal (floor), lateral and downward wall spread as opposed flow spread; and to upward wall and ceiling spread as wind-aided spread. One might argue with this lack of distinction but the opposed flow case for these different orientations has some support [8] whereas the extension of the upward spread theory to the ceiling is only a convenience for now which needs further study. For all orientations, as illustrated in Figure 2, symmetry is invoked, and the wind-aided coordinate is designated by y and the opposed flow coordinate by x . Spread on the floor (Fig. 2a), and ceiling (Fig. 2b) is radially symmetric, and on the wall (Fig. 2c) is approximated as a region developed from two linear (x and y) spreads away from an initially ignited rectilinear zone of area $2x_0y_0$. The region between the extended pyrolysis wall fronts (x_p, y_p), and the burn-out fronts (x_b, y_b) is formed by straight line approximations as illustrated in Figure 2c.

The objective of our analysis is to compute the energy release rate, $\dot{Q}(t)$, as a function of time for the orientation shown in Figure 2 or their combination. For energy release we write the following approximation based on Figure 1.

$$\dot{Q}(t) = \iint \dot{Q}'' dx dy = \bar{\dot{Q}}'' A_p \quad (1)$$

where A_p is the pyrolysis or volatilizing area.

For the floor or ceiling cases it can easily be shown that

$$A_p = \pi (x_p^2 - x_b^2) \text{ or } \pi (y_p^2 - y_b^2) \quad (2)$$

For the wall case,

$$A_p = 2 [y_p x_0 + (x_p - x_0)y_0 + 1/2 (y_p - y_0)(x_p - x_0)] \text{ for } t \leq t_b \quad (3a)$$

or

$$A_p = 2 [y_p x_0 + x_p y_0 + 1/2 (y_p - y_0)(x_p - x_0)] \text{ for } t > t_b \quad (3b) \\ - 2 [y_b x_0 + x_b y_0 + 1/2 (y_b - y_0)(x_b - x_0)]$$

In order to formulate the rest of the analysis we write out and solve the equations for the pyrolysis and burnout fronts.

Wind-aided Solution:

The upward or wind-aided solution is developed [9] from the equation

$$\frac{dy_p}{dt} = \frac{y_f - y_p}{\tau_{ig}} \quad (4)$$

where y_f is the position of the flame tip with $y_f - y_p$ defining the forward heat transfer region of the flame identified with heat flux, q_f'' . Equation (4) is a quasi-steady model which uses the steady-state flame spread result successively over time and the forward heat transfer region changes. Mathematically, this solution is continuous. This flame heat flux will be taken as 30 kW/m² in our analysis for all materials.

The ignition time is given as

$$\tau_{ig} = \frac{\pi k\rho c (T_{ig} - T_s)^2}{4 (q_f'')^2} \quad (5)$$

where T_{ig} is the ignition temperature, $k\rho c$ is the thermal inertia, and T_s is the surface temperature of the region $y \geq y_f$. As can be seen, the "property" τ_{ig} can be related to more valid engineering materials properties ($k\rho c$ and T_{ig}) and other factors.

Finally, the flame length can be estimated by a linear approximation to wall fire data [9] as

$$y_f - y_b = k_f [\dot{Q}'_o + \bar{Q}'' (y_p - y_b)] \quad (6)$$

where y_b is taken as identically zero for $t \leq t_b$, and \dot{Q}'_o is the energy release rate per unit width of the ignitor flame needed to start the process. This ignitor flame is assumed to provide a uniform heat flux $\dot{q}_f'' = 30$ kW/m² over the region (x_o, y_o) which is taken to ignite at $t = \tau_{ig}$ in Eq. (5), or corresponding to τ_{ig} in Figure 1. The value for k_f is approximately 0.01 m²/kW. In Equation (6), the term \dot{Q}'_o is set to zero after $t = t_b$. This is done after $t = t_b$ since the initial region as determined by the flame extent due to \dot{Q}'_o is no longer burning, and subsequently the ignitor flame would become discontinuous from the material flame ahead of this region. This ignitor energy is consistently included in the overall heat release.

The burnout front can be approximated as

$$\frac{dy_b}{dt} = \frac{y_p - y_b}{\tau_b} \quad \text{for } t > t_b \quad (7)$$

The initial conditions are given as:

$$t = 0, \quad y_p = y_o \quad (8a)$$

and

$$t = t_b, \quad y_p = y_p(t_b), \quad y_b = y_o. \quad (8b)$$

The solutions to the above are given below:

$$\eta = \left(\frac{a+1}{a}\right) e^{a\tau} - 1/a \quad (9)$$

for $0 \leq \tau \leq t_b/t_{ig}$ where $\tau = t/t_{ig}$, $\eta = y_p/y_o$, $a = k_f \dot{Q}'' - 1$ and $y_o = k_f \dot{Q}''_o$. This assumes that the initial pyrolysis length, y_o , is determined by the height of the ignition flame.

For $\tau > (t_b/t_{ig}) = \tau_b$. Eqns. (4) and (7) are subtracted and solved to yield

$$\psi = \frac{y_p - y_b}{y_o} = c e^{b(\tau - \tau_b)} \quad (10)$$

where $b = a - 1/\tau_b$

and $c = \left(\frac{a+1}{a}\right) [e^{a\tau_b} - 1]$.

From Eqn. (7) it follows that $\eta_b = y_b/y_o$ is given by

$$\eta_b = 1 + \frac{c}{b\tau_b} (e^{b(\tau - \tau_b)} - 1) \quad (11)$$

The parameters a and b must be greater than zero in order for the upward fire spread to accelerate. For values less than zero, the spread will eventually stop. This bimodal behavior is a distinct characteristic of upward flame spread which is conditional on the form of Eqn. (6). This clearly shows the role of the energy release rate per unit area and its duration in time, i.e., \dot{Q}'' and t_b .

Opposed flow solution:

From the LIFT procedure [2,6] the governing equation for the pyrolysis position is

$$\frac{dx_p}{dt} = \frac{\Phi}{k\rho c (T_{ig} - T_s)^2} \text{ for } T_s \geq T_{s,min}. \quad (12)$$

This can be rewritten as

$$\frac{dx_p}{dt} = \frac{\pi \Phi}{4 (q_f'')^2 t_{ig}} \quad (13)$$

The dimensionless solution $\xi = x_p/x_o$ follows as

$$\xi = \beta\tau + 1 \quad (14)$$

where $\beta = \frac{\pi \Phi x_o}{4 (q_f'')^2}$

The burnout solution analogously follows from Eqn. (7), i.e.

$$\frac{dx_b}{dt} = \frac{x_p - x_b}{t_b}, \quad (15)$$

and it can be shown that $\xi_b = x_b/x_o$ is given by

$$\xi_b = \beta (r - \tau_b) + 1, \quad r \geq \tau_b. \quad (16)$$

This completes the solution. These equations will now be applied to specific applications. For each case we shall appropriately apply the equations by accounting for the effects of geometry and thermal feedback as a parameter. For example, a corner wall and ceiling fire will be considered as an extended vertical wall representative of the actual upward and wall ceiling jet region plus a quadrant of a circular ceiling.

To review, the procedure for implementing this solution is as follows:

1. Assemble material data namely, \bar{Q}'' , t_{ig} , t_b , Φ and $T_{s,min}$.
2. Prescribe the ignition source, \dot{Q}'_o .
3. Since no room fire model is coupled to this analysis, one must set T_s to a value representative of the particular room configuration.
4. Compute the pyrolysis area A_p for the surface configuration using the formulas for x_p and y_p .
5. Compute the fire product output rate, e.g. rate of any energy release, by multiplying A_p by \dot{Q}' .

3. APPLICATIONS

Several applications of the analysis will be presented for cases where scenario results for total energy release exist along with a complete set of fire property data.

3.1 Full Scale Room - Corner Tests

A series of full scale room lining fire tests were performed at the Swedish National Testing Institute, Borås, Sweden [10]. The test scenario consisted of lining the walls and ceiling of the room (2.43 m by 3.66 m by 2.43 m in height with an opening 2 m by 0.9 m) with a given material. A 0.17 m by 0.17 m sand burner was placed in the corner of the full scale room. Initially a 100 kW fire was allowed to burn in the corner. If this fire did not cause flashover in 10 minutes, then the burner output was increased to 300 kW.

Small scale fire test data were obtained by other researchers for the materials used in the Borås study [5,11,12] and were used to develop Table 1. These values are used for the model inputs. In the calculations, ceiling fire spread is accounted for by having the ceiling ignite when the pyrolysis front

reaches the ceiling. The ceiling spread follows the wind-aided spread along the wall ceiling interface. Thus, the pyrolyzing ceiling area is given as the quadrant of the ceiling with the radius equal to the distance from the corner to the wall ceiling interface pyrolyzing front. Lateral spread was deemed to occur only when the wall surface temperature is at the material's $T_{s,min}$ or greater. The model was run with T_s at 25°C and 80°C. While at the start of the experiment the surface temperature is uniform (approximately 25°C) throughout, allowing T_s to be an input parameter shows the sensitivity to feedback and the effects which increased lateral spread has on the results. This is justified because, while early on in the test T_s of 25°C is more representative of the room conditions, the upper layer temperature is always increasing and radiative feedback is raising wall and ceiling temperatures. We selected burner flame heights (y_o) of 1.3 m and 2.1 m for the 100 and 300 kW settings. We determined y_o values from an axisymmetric fire plume correlation realizing that corner flames would be taller and ignoring ceiling interaction. For cases that stopped propagating before 10 minutes, the analysis was restarted at $t=600$ s from a new origin at $y_b(600$ s). If $y_b(600$ s) is greater than 2.1 m, the ignitor flame height, we arbitrarily selected 0.3 m as a new y_o in order to initiate spread again. Also for $t > 600$ s, we selected $T_s = 250^\circ\text{C}$ based on the maximum gas temperatures measured [10]. Model predictions and experimental results for the time to a 1 MW fire are given in Table 2. Figure 3 shows the experimental rate of heat release as a function of time (solid curves) and model calculations (dashed curves) with $T_s = 80^\circ\text{C}$ for three of the materials. Appendix A contains plots of experimental rate of heat release and model calculations for all 13 materials. The results are comparable to those of Karlsson (who only considered 6 of the materials) [5], but appear to be distinctly better than the results of Wickström and Göransson [3].

3.2 PMMA Room Wall Test

A PMMA wall fire test was performed at NIST [13]. The wall opposite the doorway of an enclosure of roughly the same dimension as the Borås room was lined with 12.7 mm thick clear PMMA, and a small line burner 0.3 m wide was placed at floor level in the center of the wall. The igniter flame height was nominally 0.15 m. The pyrolysis area as a function of time was recorded from video records and imbedded thermocouples. Initially, the fire spreads up the wall, and across the wall-ceiling interface (ceiling jet). This mode of spread is characterized as wind-aided spread. As this is occurring, lateral spread is extending the initial pyrolyzing width of 0.3 m. Appendix B shows the measured surface temperatures at different position and the estimated pyrolysis area.

The model input values for this PMMA wall fire are burning rates of 6, 7, and 8 $\text{g/m}^2\text{s}$ (multiplied by 25 kJ/g for rate of heat release), 160 s for $t_{i,g}$ (this assumes a value of 380°C for $T_{i,g}$, 1.02 $(\text{kW/m}^2\text{K})^2\text{s}$ for $k\rho c$, and q_f of 25 kW/m^2), t_b of 1000 s, and Φ of 14.4 kW^2/m^3 . The minimum temperature for lateral spread is approximately 25°C for this material. With these input values, the pyrolysis area is calculated as a function of time for the three different burning rates. These burning rates are representative of unenhanced wall burning rates which would be applicable before significant thermal feedback occurs. The results are shown in Figure 4. The model results with

input burning rates of 6 and 8 g/m²s bound the measured pyrolysis area while 7 g/m²s compares well up to 700 s. The calculated areas start to level off after the pyrolysis front reaches the ends of the wall (laterally) at the wall-ceiling interface. The experimental results show a rapid increase in pyrolysis area due to a fast downward spread. This is due to the thermal feedback of the hot layer increasing the surface temperature of the wall, thus increasing downward spread. This feedback is not explicitly accounted for in the model, therefore, we do not expect to match the experimental results at long times. Also we have used burning rates for PMMA associated with no external irradiance. This is in contrast to our use of Cone Calorimeter data at irradiance levels of 25 kW/m² and higher for corner fire tests.

3.3 Textile Wall Covering Room Tests

A series of textile wall fire tests was performed by the U.C., Berkeley for the American Textile Manufacturers Institute [14]. In these tests, 0.31 m (1 ft) and 0.62 m (2 ft) wide strips of different textile wall covering materials were applied to a corner section and the wall portion of the wall-ceiling interface of a room with roughly the same dimensions of the room used in the tests above. A 0.31 m by 0.31 m sand burner was placed in the material lined corner approximately 10 cm from the walls. A small 40 kW fire was allowed to burn in the corner for 5 minutes, then the burner output was increased to 150 kW. The position of the burner and the size of the small 40 kW fire was such that in most cases it did not cause the textile material to ignite, but shortly after the burner output was increased to 150 kW, all wall lining materials ignited. The rate of heat release was obtained during each test. The data for input into the model is given by Harkleroad [15]. Here lateral spread was not included in the calculations since lateral spread is not expected with the 0.31 m wide strips anyway. It appears from the experimental results that the 40 kW fire only served to preheat the room, therefore we picked an initial surface temperature of 100°C based on the maximum gas temperatures measured during this preheating time. In the experiments, there appears to be very little ignition delay of the materials after the burner output is increased to 150 kW. This is due to the preheating by the small 40 kW fire, and the high heat flux from the 150 kW fire. Table 3 shows the experimental and calculated results. By examining the 0.31 m and 0.62 m wide strip results, it appears in some cases lateral spread is significant. The model calculations were performed for the 0.31 m wide strip cases using Cone Calorimeter data at external irradiances of 30 and 50 kW/m². Ignition delay times for each of the materials were calculated from Eq. (5). For this calculation, we assumed $T_s = 100^\circ\text{C}$ and $\dot{q}_f'' = 60 \text{ kW/m}^2$ which represents the high heat flux produced by the ignitor [16], and added this calculated ignition time to the model calculated time to reach the peak rate of heat release. The peak heat release rate and the time interval from the start of the 150 kW fire for the 0.31 m strips compare favorably with the calculations. After the peak heat release was obtained a rapid decay was observed experimentally for most cases, this was predicted well by the model.

4. CONCLUDING REMARKS

We have presented evidence that an engineering approach utilizing "fire property" data from test methods can satisfactorily predict full scale energy release of room lining fires. The fire properties used are not necessarily fundamental engineering data, but the analysis does not preclude the use of such properties. Consequently, the choice of the fire properties used is somewhat arbitrary until the fire heat transfer conditions can be related to the test method irradiance levels. Also the model used to make the predictions, although yielding reasonably satisfactory results, should be refined and improved. Nevertheless, the framework presented should serve as a basis for these improvements and might be used now to more rationally assess the fire growth hazard of lining materials.

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Nomenclature

A	area
a	dimensionless parameter, Eq. (9)
b	dimensionless parameter, Eq. (10)
c	dimensionless parameter, Eq. (10)
$k\rho c$	thermal inertia (thermal conductivity x density x specific heat)
k_f	constant, $0.01 \text{ m}^2/\text{kW}$, Eq. (6)
q	heat transfer
Q	energy
t	time
t	temperature
x	opposed flow coordinate direction
y	wind-aided coordinate direction
β	dimensionless parameter, Eq. (14)
τ	dimensionless time, t/t_b
ξ	dimensionless pyrolysis position, x_p/x_o
ξ_b	dimensionless burnout position, x_b/x_o
η	dimensionless pyrolysis position, y_p/y_o
η_b	dimensionless burnout position, y_b/y_o
Φ	flame heating parameter, Eq. (12)

Subscripts:

b	burnout
f	flame
ig	ignition
o	initial
p	pyrolysis

Superscripts:

($\bar{\quad}$)	average
($\dot{\quad}$)	per unit time
(\prime)	per unit width
($\prime\prime$)	per unit area

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Table 1

Flame Spread and Heat Release Properties of Swedish Fire Test Materials

Material	T_{ig} (°C)	$k\rho c$ (kW/m ² K) ² s	Φ (kW ² /m ³)	$T_{s,min}$ (°C)	\bar{Q}'' (kW) (25 kW/m ²)	t_b (s)	\bar{Q}'' (kW) (50 kW/m ²)	t_b (s)
Particle Board	405	0.626	8	180	140	>500	200	>500
Insulating Fiberboard	381	0.229	14	90	120	>500	150	>300
Medium Density Fiberboard	361	0.732	11	80	140	>500	170	>600
Wood Panel (Spruce)	389	0.569	24	155	140	>200	160	>400
Melamine Covered Particle Board	483	0.804	<1	435	-	-	115	>400
Paper Covered Gypsum Board	388	0.593	0.5	300	100	40	200	20
PVC Covered Gypsum Board	410	0.208	25	300	105	20	160	20
Textile Covered Gypsum Board	406	0.570	9	270	200	30	300	20
Textile Covered Mineral Wool	391	0.183	6	174	250	30	375	20
Paper Covered Particle Board	426	0.680	13	250	140	>500	150	>500
Polyurethane Foam (rigid)	393	0.031	3	105	110	60	180	60
Expanded Polystyrene	482	0.464	-	-	-	-	300	100
Gypsum Board	469	0.515	14	380	-	-	100	20

- Data were not taken

Table 2

Time to Achieve a 1 MW Fire for the Swedish Room Tests

Material	Experimental Time (s)	Model Calculations		
		Irradiance 25 kW/m ² (T _s = 25°C) (s)	Irradiance 50 kW/m ² (T _s = 25°C) (s)	Irradiance 25 kW/m ² (T _s = 80°C) (s)
Particle Board	157	198	143	145
Insulating Fiberboard	59	77	58	55
Medium Density Fiberboard	131	180	148	125
Wood Panel (Spruce)	131	165	143	117
Melamine Covered Particle Board	465	-	402	-
Paper Covered Gypsum Board	640	632	616	641
PVC Covered Gypsum Board	611	619	606	622
Textile Covered Gypsum Board	639	615	613	615
Textile Covered Mineral Wool	43	33	28	24
Paper Covered Particle Board	143	237	220	177
Rigid Polyurethane Foam	6	11	6	7
Expanded Polystyrene	115	-	122	-
Gypsum Board	*	-	*	-

- Data were not taken

* Did not Reach 1 MW

Table 3

Textile Wall Coverings Room Fire Tests

MATERIAL	Full Scale Screening Tests				Model Calculations			
	0.31 m Strips		0.62 m Strips		Irradiance 30 kW/m ²		Irradiance 50 kW/m ²	
	\dot{Q}_p (kW)	t_p^* (s)	\dot{Q}_p (kW)	t_p^* (s)	\dot{Q}_p (kW)	t_p^* (s)	\dot{Q}_p (kW)	t_p^* (s)
(H) 85% wool 15% cotton	46	30	160	40	-		146	46
(C) 55% cotton 45% rayon	62	30	119	60	137	40	139	37
(G) 100% polyester	83	30	-		64	39	56	44
(B) 100% polyester	207	45	298	60	121	46	270	46
(Q) 100% polyester	207	40	480	40	145	50	293	55
(Qfr) 100% polyester	310	40	-		157	43	292	59
(R) 100% nylon	587	70	590	70	46	46	416	51
(AA) 70% acrylic 30% wool	684	30	-		725	109	744	106
(PPPF) polypropylene	-		337	50	271	45	450	48

- Data were not taken \dot{Q}_p = peak energy release rate

t_p^* = time interval from start of 150 kW burner to peak energy release rate

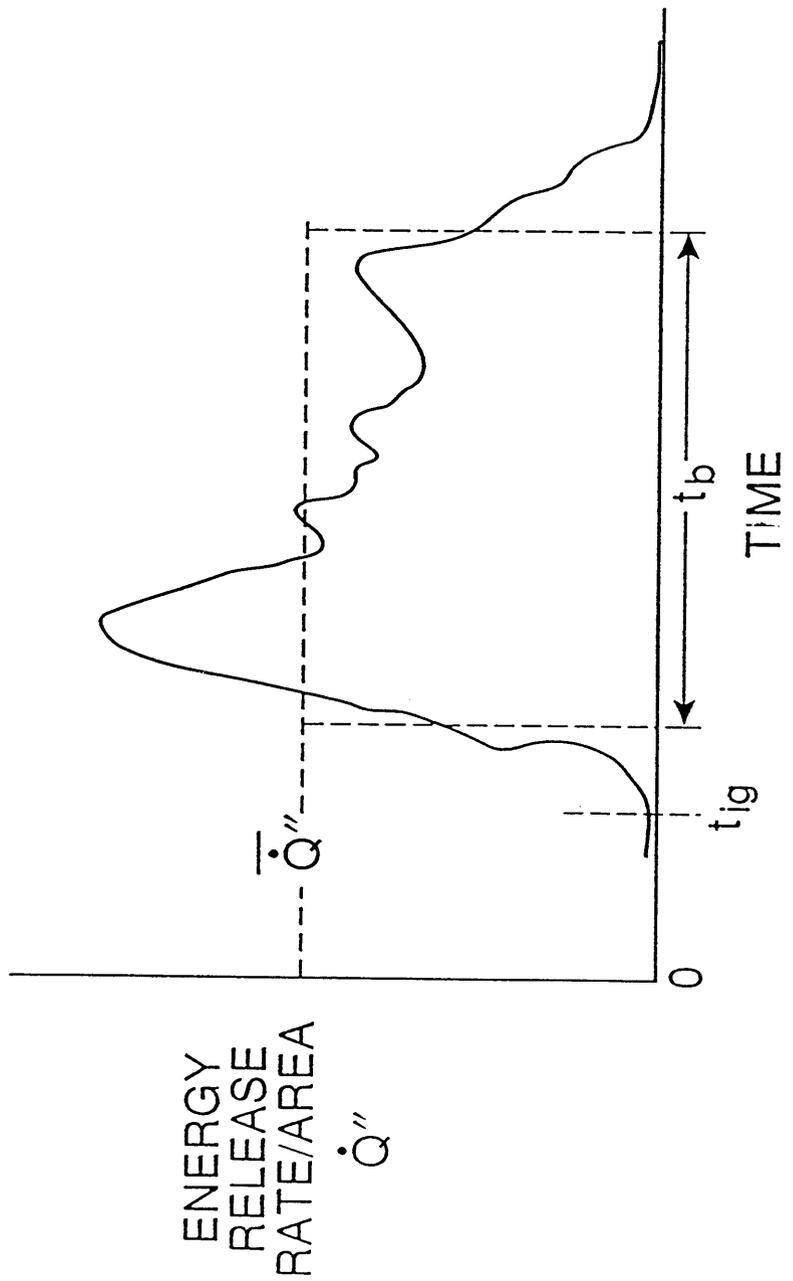


Figure 1. Energy release property data.

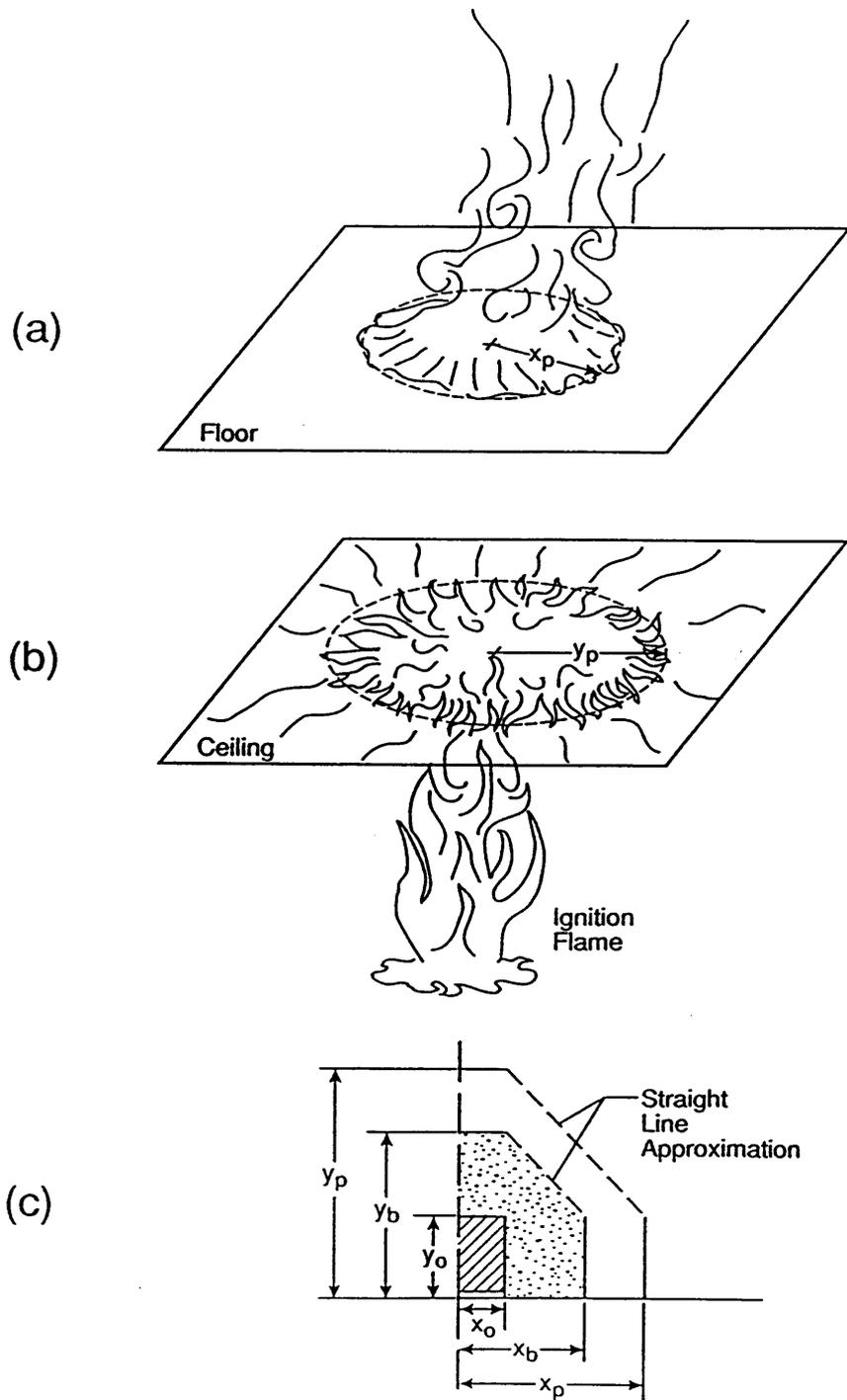


Figure 2. Model floor, ceiling and wall configurations

FULL SCALE ROOM CORNER TESTS

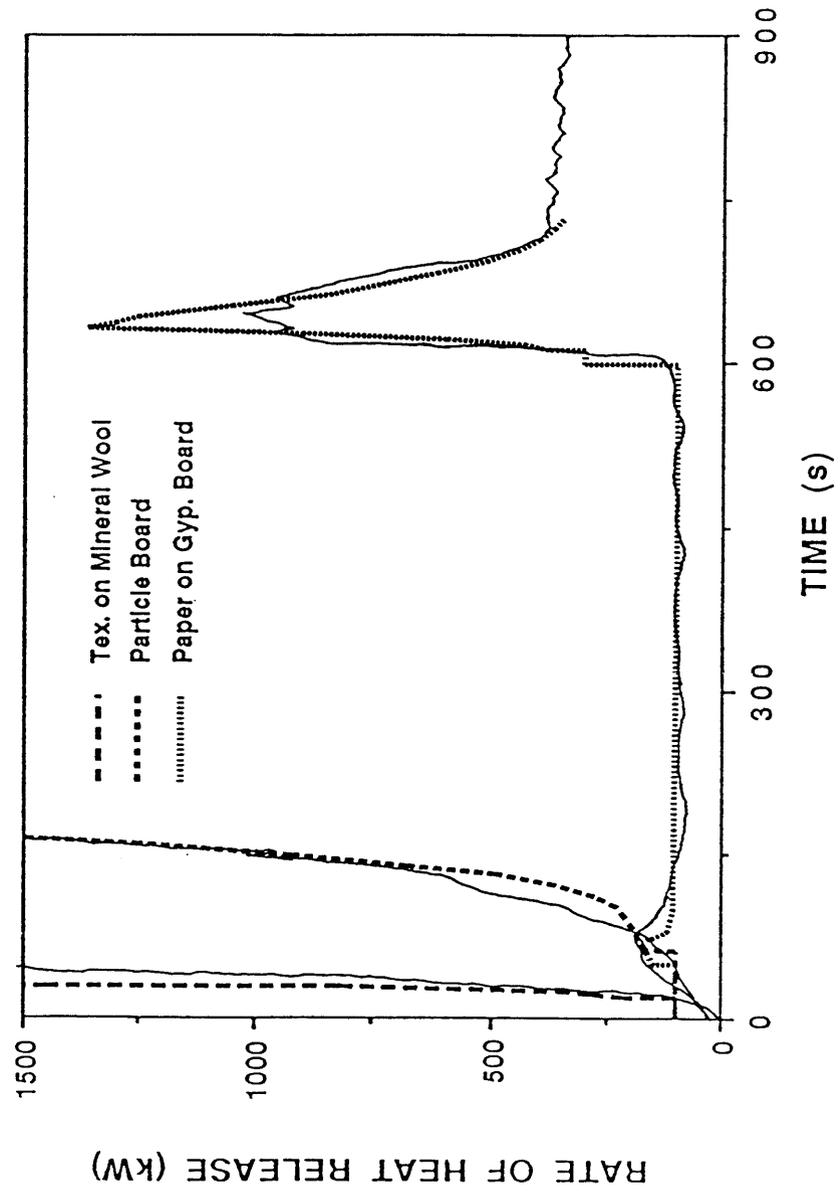


Figure 3. Energy release predictions for the Borås data

PMMA ROOM WALL TEST

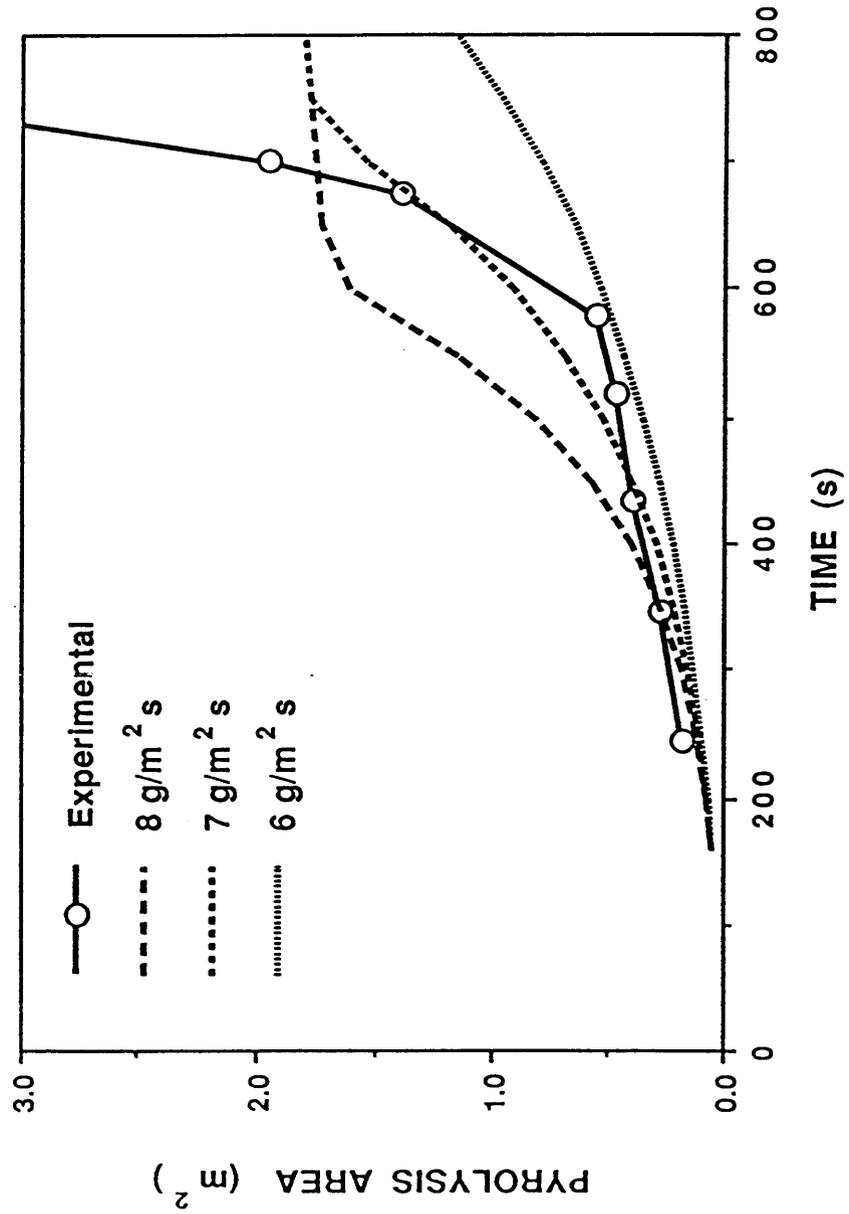


Figure 4. Growth of the pyrolysis area on a PMMA wall

Appendix A. Full Scale Room-Corner Tests

The experimental results and model predictions for the twelve materials examined at the Swedish National Testing Institute are shown in figures A-1 to A-12. Model calculations with $T_s = 25^\circ\text{C}$ and 80°C are both presented. Data from the Cone Calorimeter at an irradiance of 25 kW/m^2 was used for these calculations with the exception of Melamine-faced particle board and Polystyrene where Cone Calorimeter data at an irradiance of 50 kW/m^2 were used.

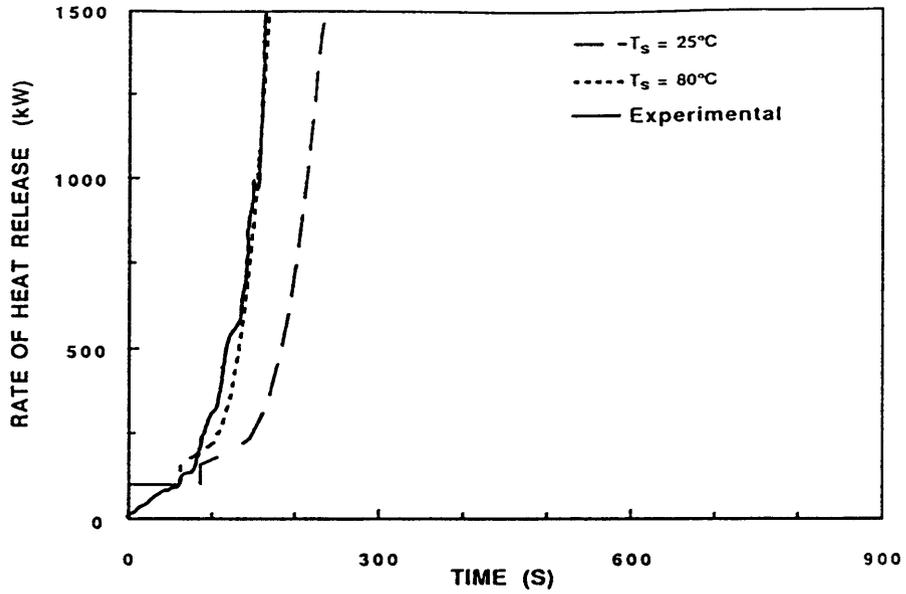


Figure A-1. Rate of heat release vs. time for particle board lined room

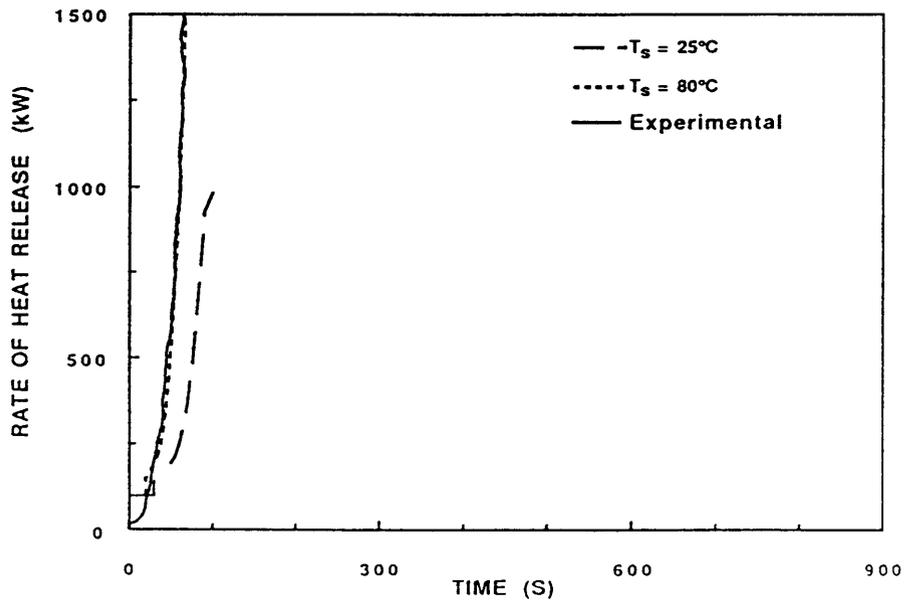


Figure A-2. Rate of heat release vs. time for insulating fiberboard lined room fire

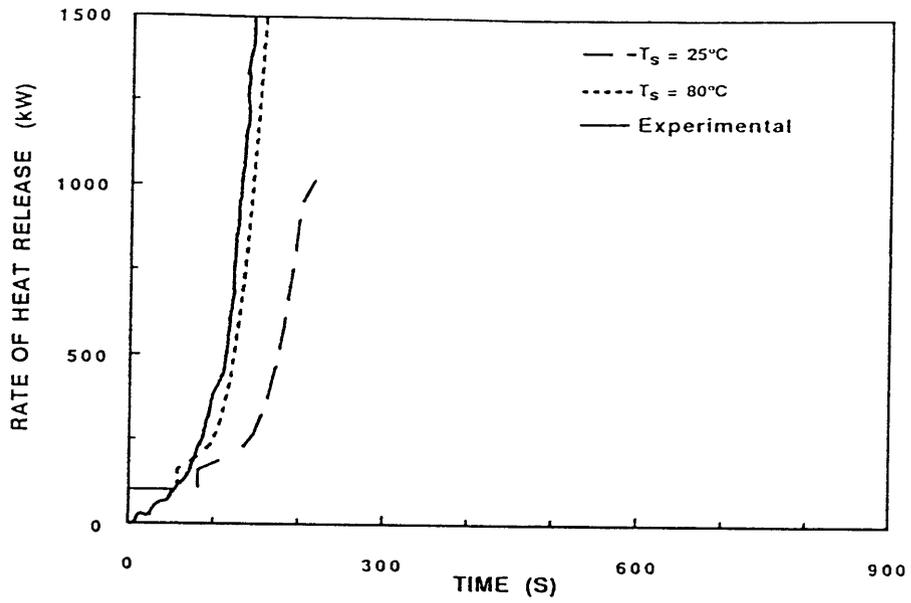


Figure A-3. Rate of heat release vs. time for medium density fiberboard lined room fire.

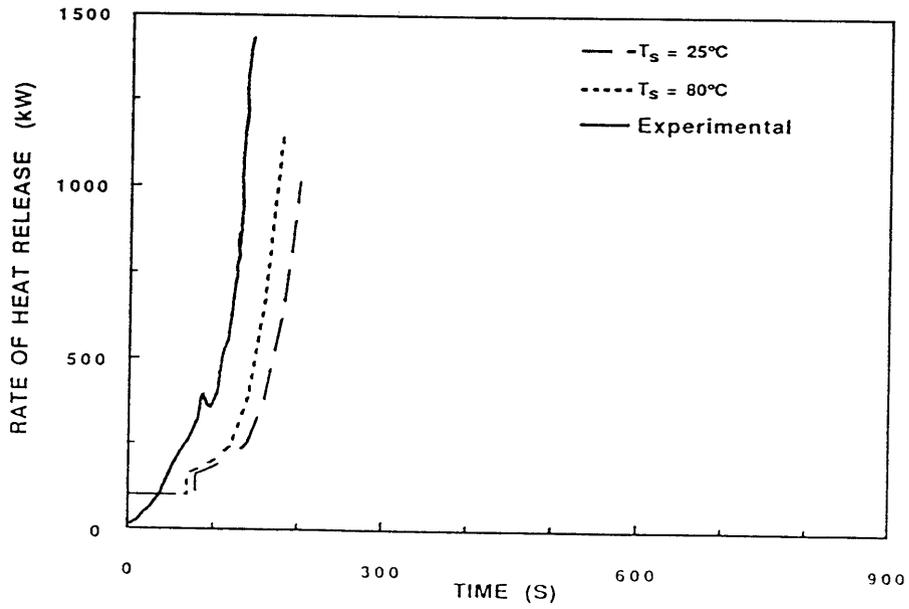


Figure A-4. Rate of heat release vs. time for wood paneling lined room fire.

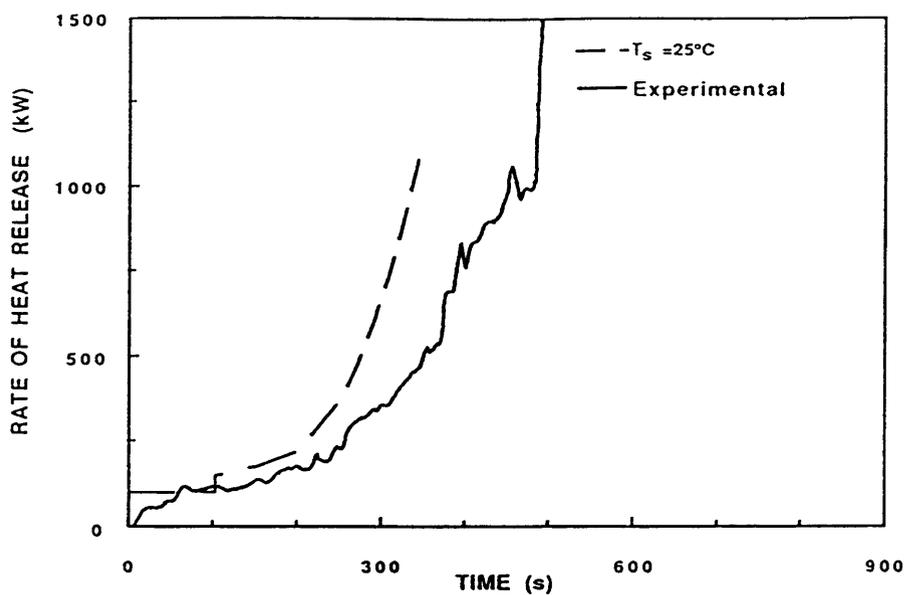


Figure A-5. Rate of heat release vs. time for melamine faced particle board lined room fire.

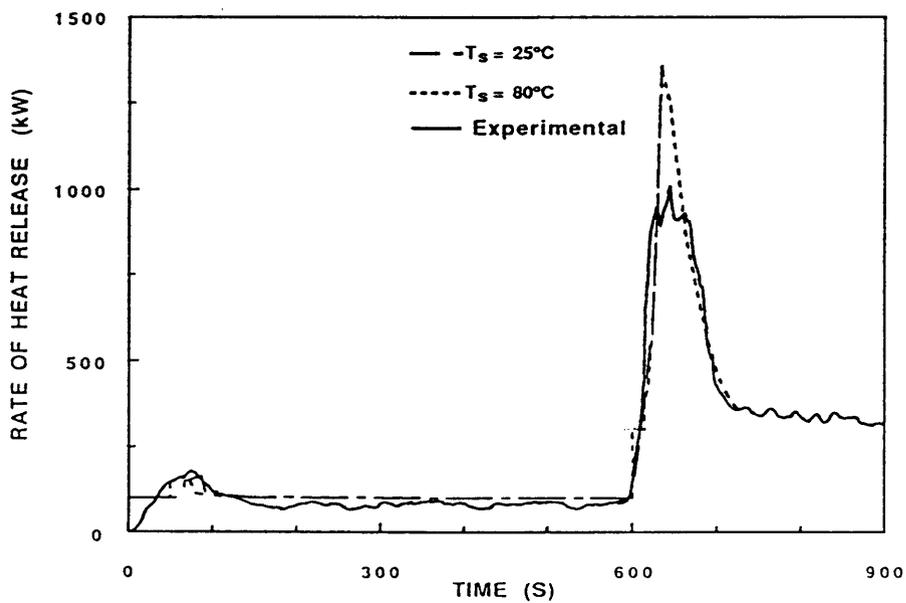


Figure A-6. Rate of heat release vs. time for paper covered gypsum board room fire.

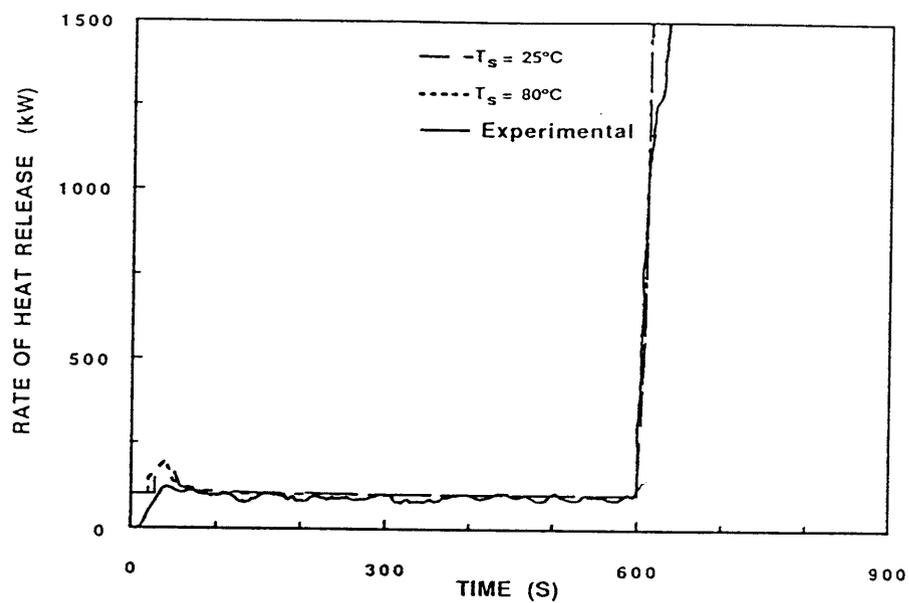


Figure A-7. Rate of heat release vs. time for pvc covered gypsum board room fire.

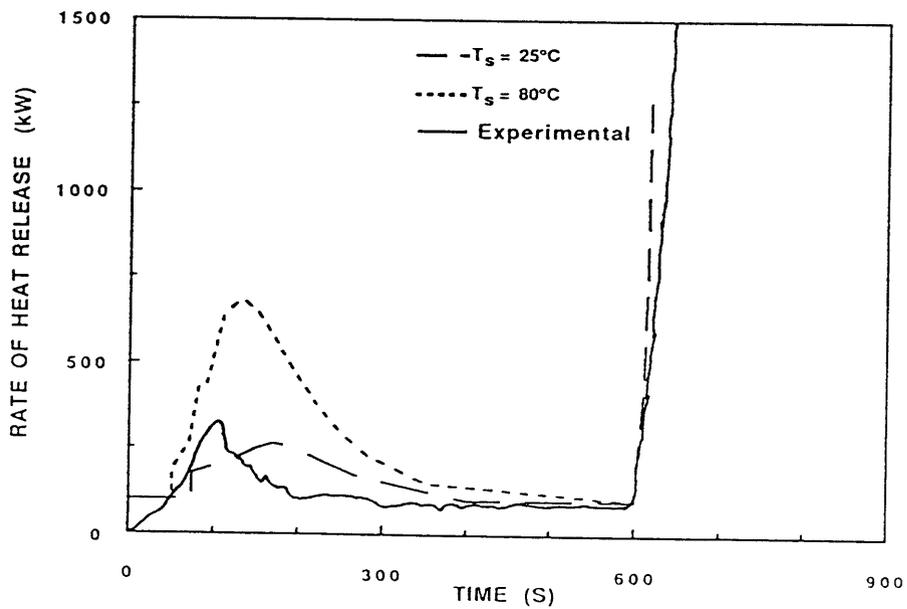


Figure A-8. Rate of heat release vs. time for textile wallcovering on gypsum board lined room fire.

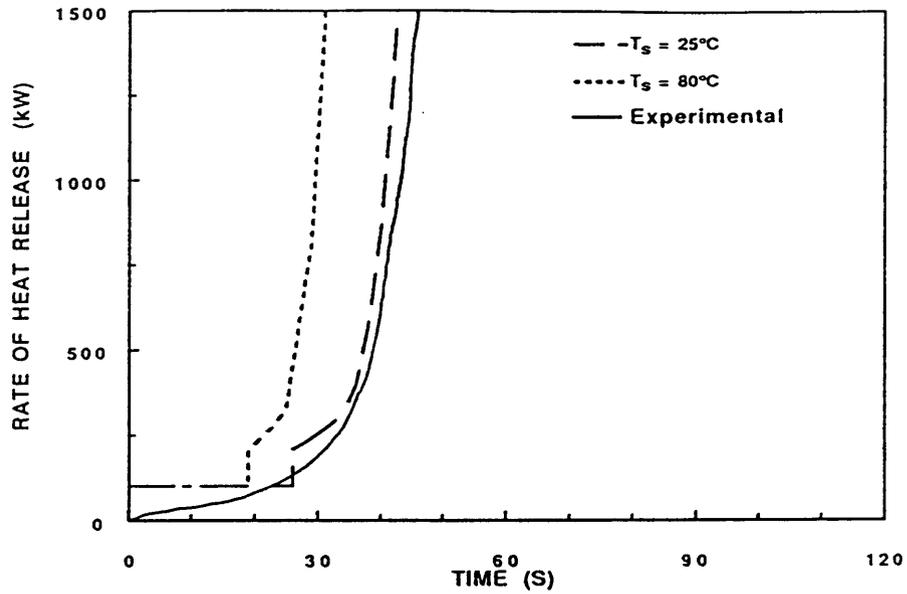


Figure A-9. Rate of heat release vs. time for textile wallcovering on mineral wool lined room fire.

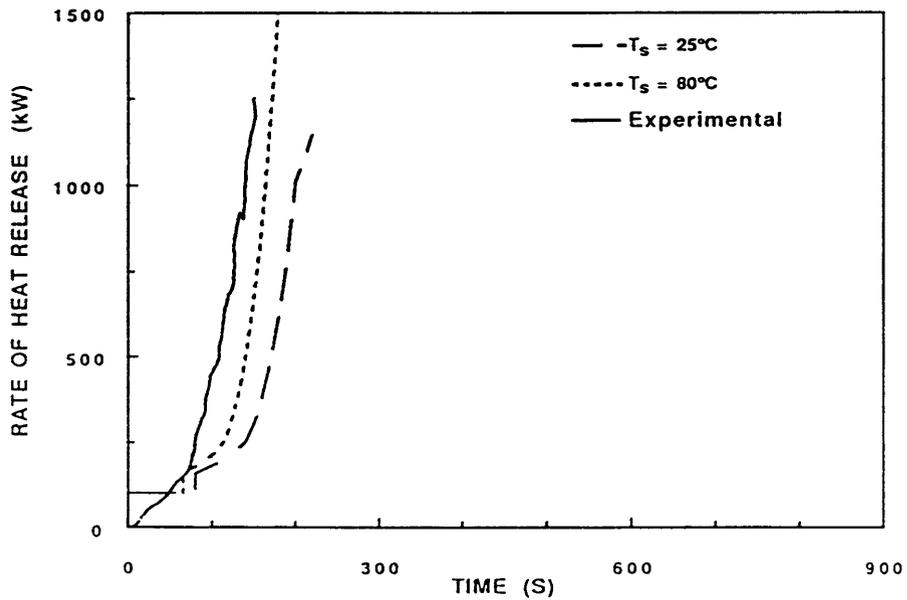


Figure A-10. Rate of heat release vs. time for paper covered particle board lined room fire.

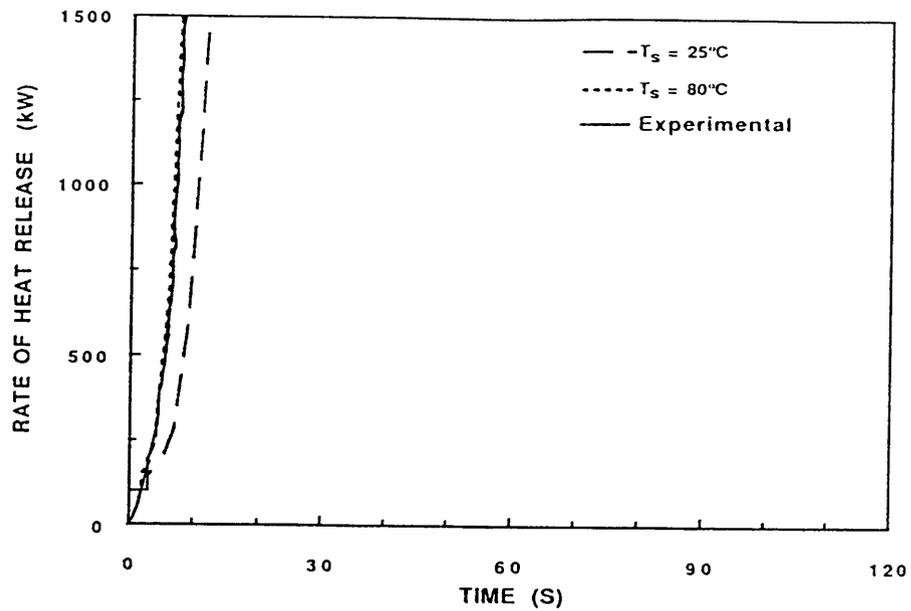


Figure A-11. Rate of heat release vs. time for rigid polyurethane foam lined room fire.

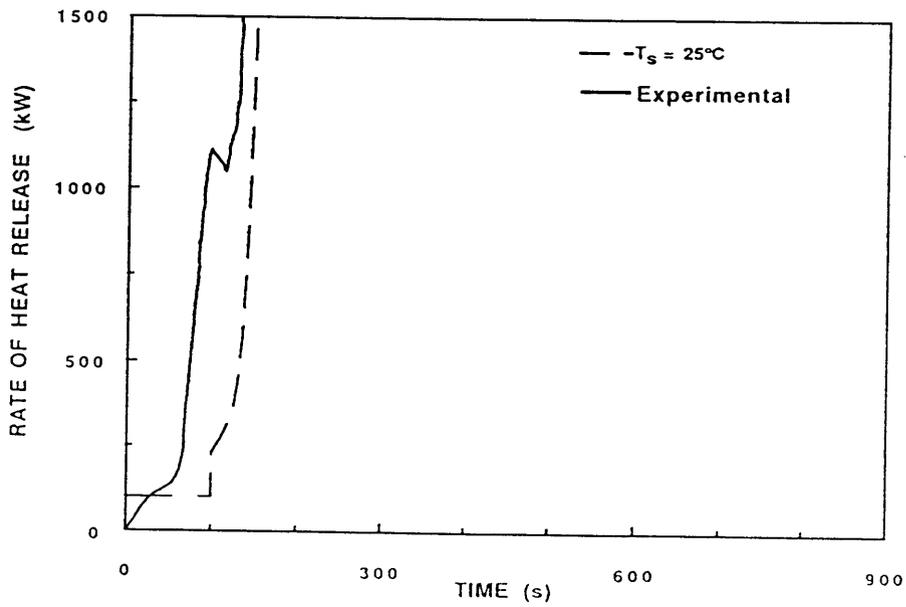


Figure A-12. Rate of heat release vs. time for expanded polystyrene lined room fire.

Appendix B. PMMA Room Wall Fire Test

Figure B-1 shows surface temperature measurements for a PMMA room wall fire performed at NIST [12]. The (x) symbols denote the locations of the 0.25 mm chromel-alumel thermocouples, the (o) symbols denote the locations of heat flux gages. The numbers indicate the time in seconds from the start of the test to the time when the thermocouple reads a surface temperature of 378°C. This temperature is used as the critical surface temperature at ignition. The underlined numbers indicate the time in seconds for the heat flux gage to register a heat flux of 15 kW/m². Table B-1 is an estimate of pyrolysis area as a function of time for this experiment. These values are plotted in Figure 4 as the experimental values.

Table B-1

Pyrolysis area estimated from thermocouple data

Time (s)	Pyrolysis Area (m ²)
245	0.19
345	0.28
435	0.40
520	0.47
580	0.56
675	1.39
700	1.95
750	3.62
800	4.18

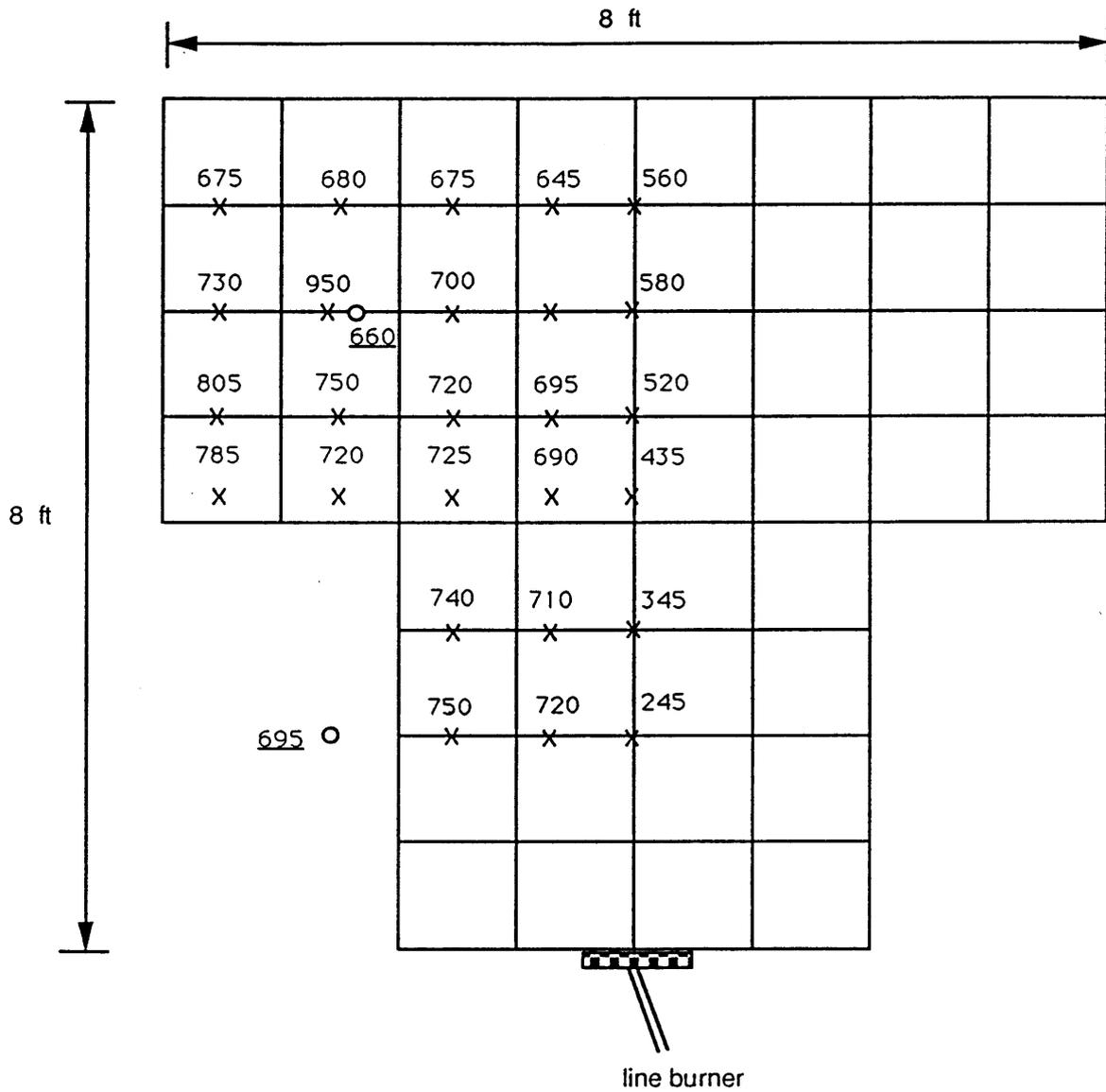


Figure B-1. Time to reach ignition temperature at various positions for flame spread on a PMMA wall section in an enclosure.

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11. ABSTRACT (A 200-WORD OR LESS FACTUAL SUMMARY OF MOST SIGNIFICANT INFORMATION. IF DOCUMENT INCLUDES A SIGNIFICANT BIBLIOGRAPHY OR LITERATURE SURVEY, MENTION IT HERE.) A complete approximate set of equations is developed to describe fire spread and its resultant energy release over a surface. Wall, floor, and ceiling orientations are considered. The needed model data are couched in terms of available test method results, e.g., Cone Calorimeter and LIFT apparatuses. Several applications are presented to show how energy release rates can be predicted and how well they represent real data from full-scale and model room lining experiments.										
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